

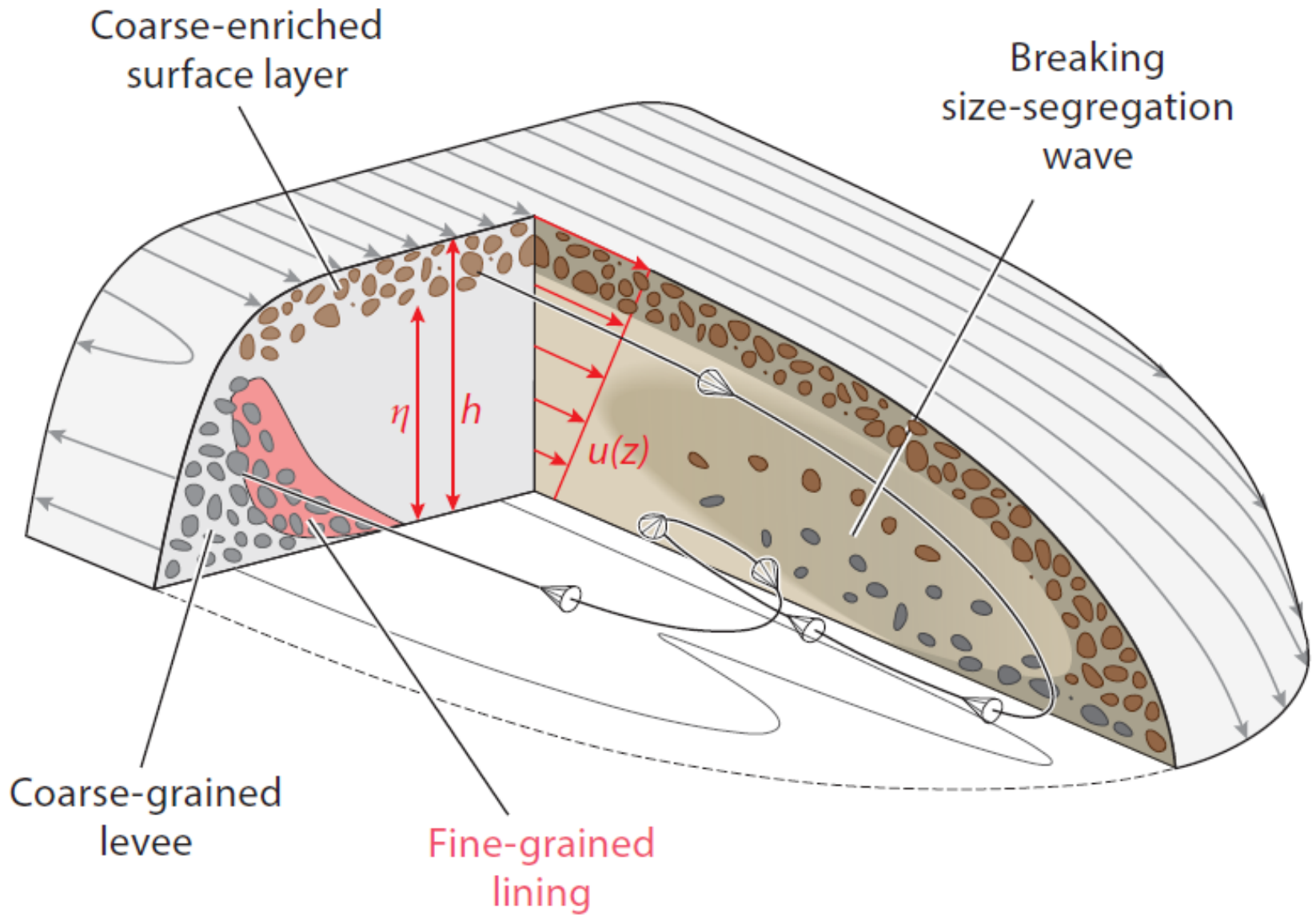
# Particle segregation and rheology of dense granular flows

Nico Gray



Johnson *et al* (2012) *J. Geophys. Res.* **117**, F01032





- larger particles are shouldered to the sides to create levees
- this is an example of a segregation-mobility feedback effect

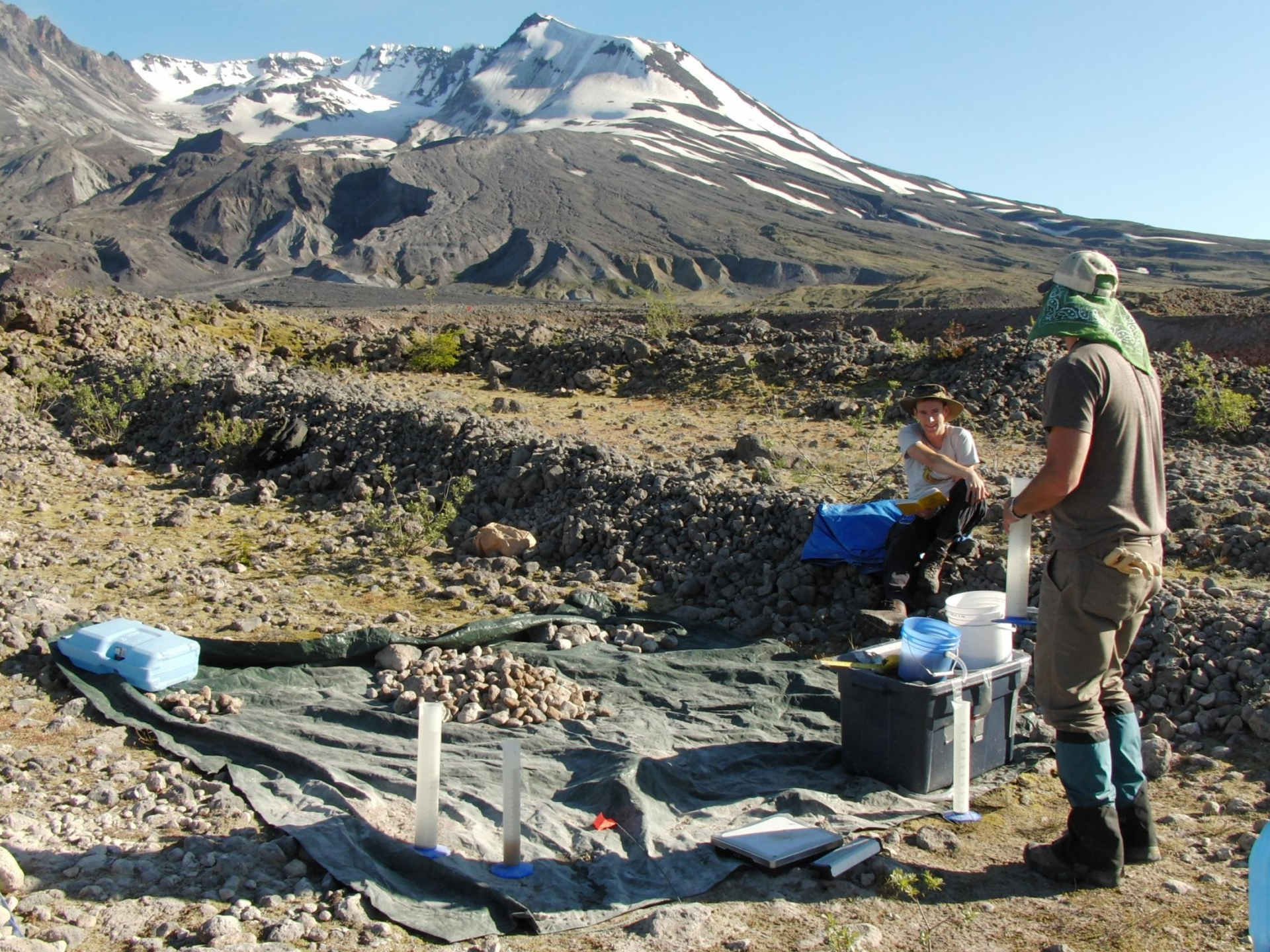
Mount St Helens, USA, 1980

Finer grained interior

Coarse rich levee



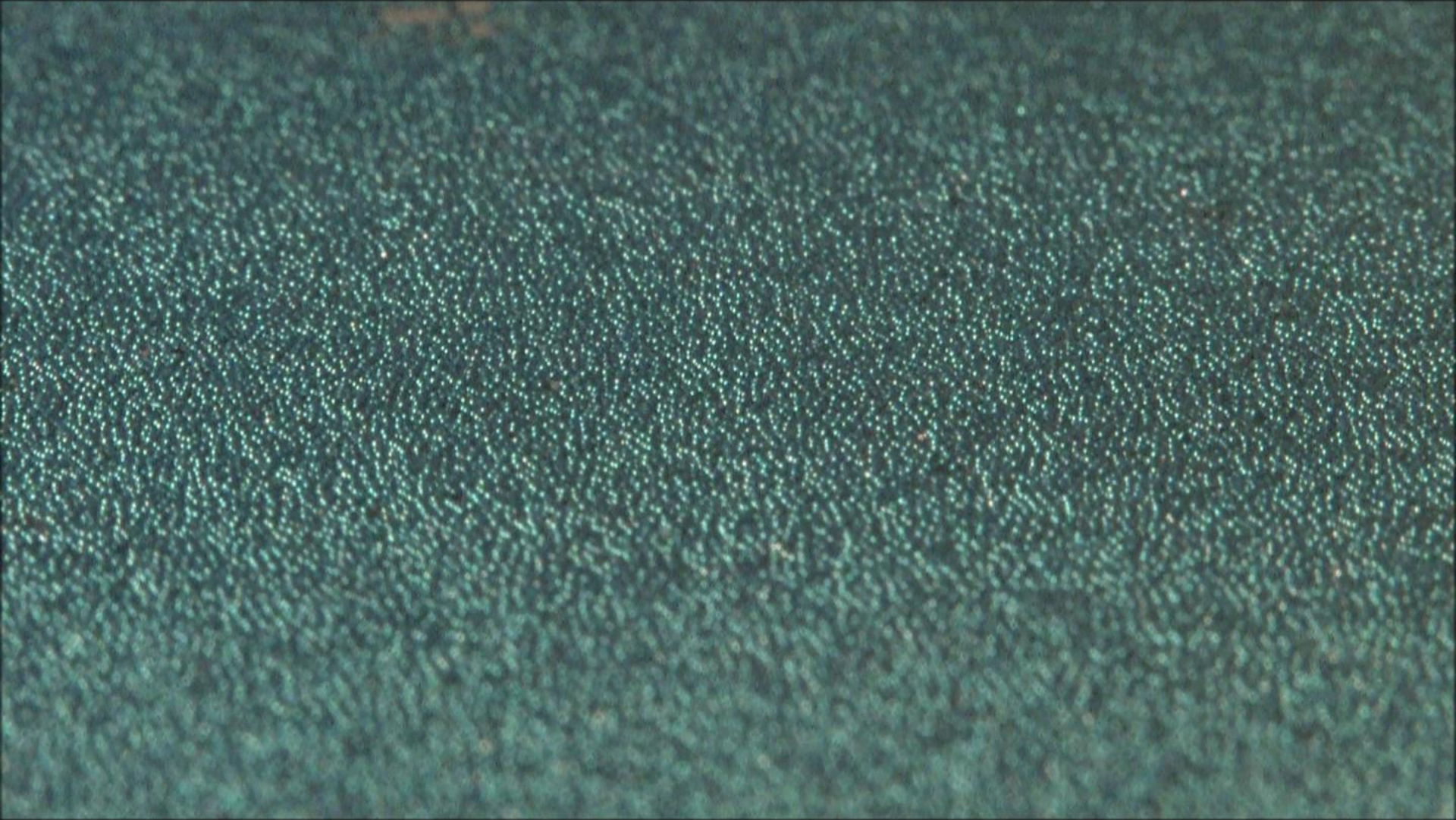
- segregation occurs in many hazardous natural flows
  - debris-flows, pyroclastic flows & snow avalanches
- and leads to spontaneous flow organization and longer run-out



## Segregation induced finger formation ...

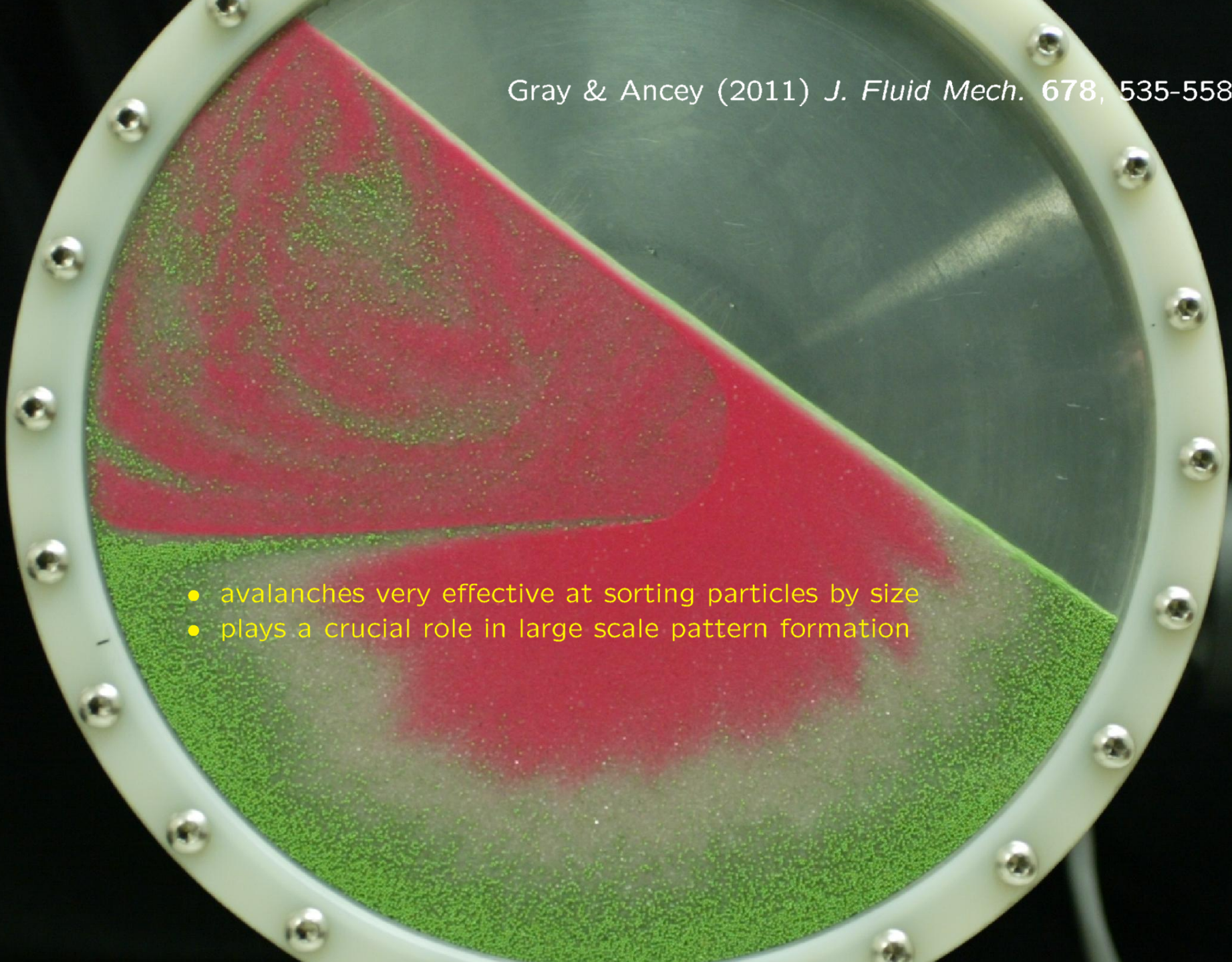


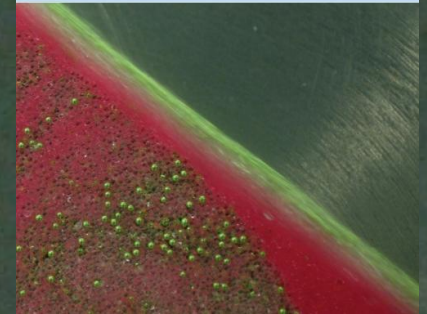
Pouliquen, Delours & Savage (1997), *Nature*. **386**, 816-817.  
Woodhouse *et al.* (2012), *J. Fluid Mech.* **709**, 543-580.



Woodhouse *et al.* (2012), *J. Fluid Mech.* **709**, 543-580.  
Kokelaar *et al* (2014) *Earth Planet. Sci. Lett.* **385**, 172-180.

- avalanches very effective at sorting particles by size
- plays a crucial role in large scale pattern formation



 $z$ 

$$|u = (u, w)$$

 $x$ 

Slowly rotating mixture

Large

Medium

Small

Surface avalanche

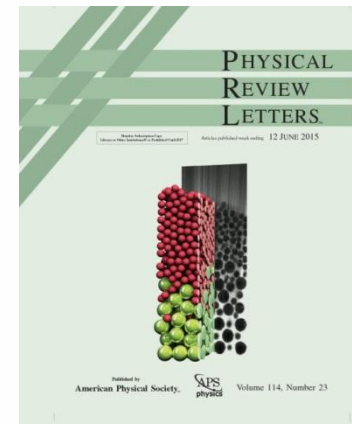
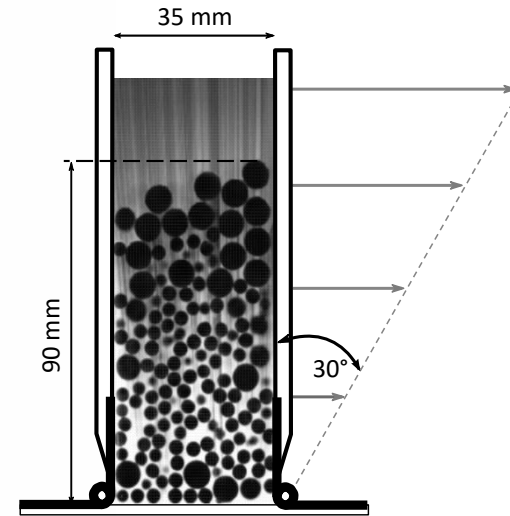
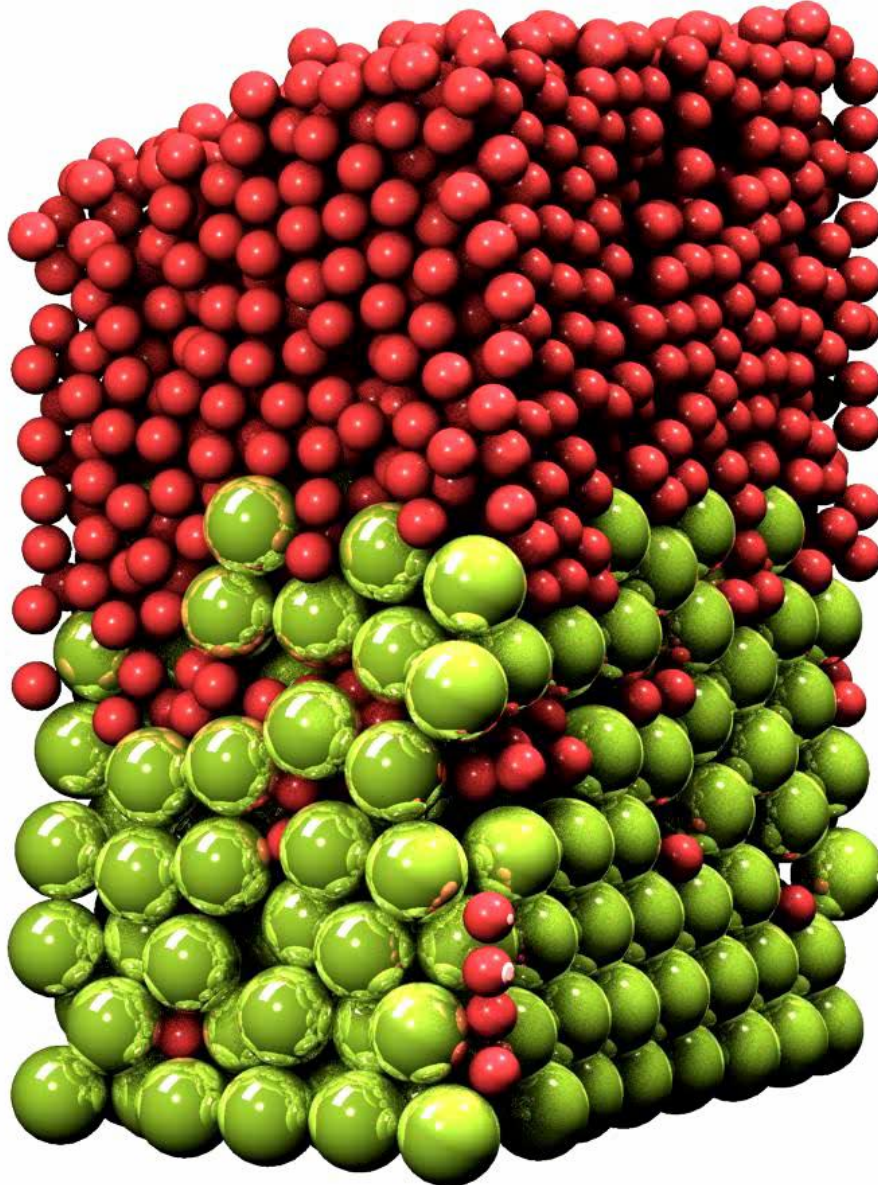
 $\zeta$ 

### Kinetic sieving and squeeze expulsion

- small particles fall down into gaps
- and then force large particles up
- to create inversely graded layers



# Index matched shear box experiments on bi-disperse segregation



2 Bi-disperse segregation equation for small particle concentration A is

$$\frac{\partial \phi}{\partial t} + \nabla \cdot (\phi \mathbf{u}) + \frac{\partial}{\partial z} (-S_r F(\phi)) = \frac{\partial}{\partial z} \left( D_r \frac{\partial \phi}{\partial z} \right)$$

2 where bulk velocity  $u$ ,  $S_r$  is the segregation rate and  $D_r$  is the diffusion

2 The segregation flux  $F = F(\phi)$  satisfies the constraints that

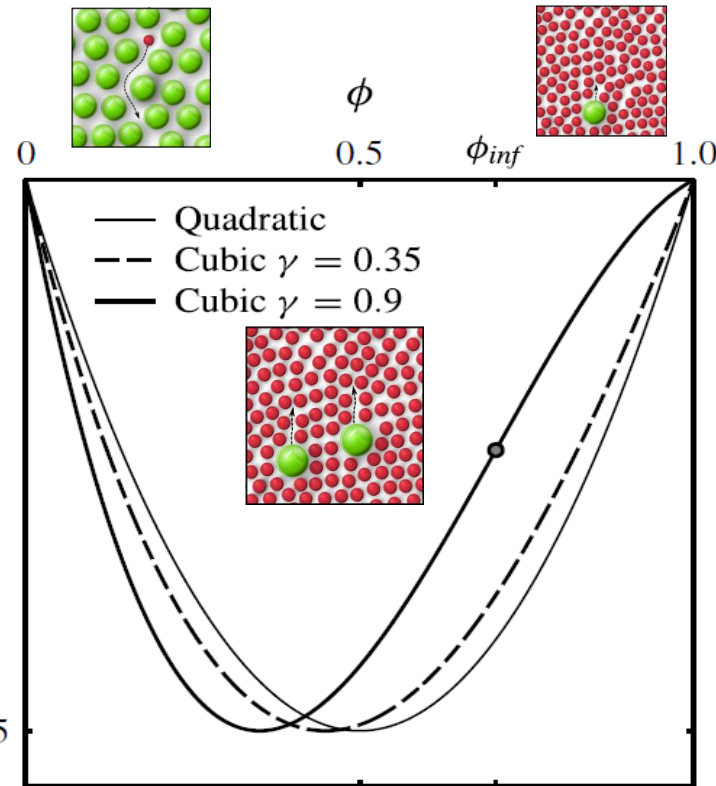
$$\left. \begin{aligned} F = 0, \quad \phi = 0, \\ F = 0, \quad \phi = 1. \end{aligned} \right\}$$

2 Gray & Thornton (2005)

$$F(\phi) = \phi(1 - \phi)$$

2 Gajjar & Gray (2014)

$$F(\phi) = A_\gamma \phi(1 - \phi)(1 - \gamma\phi), \quad -F(\phi)$$



Bridgwater, Foo & Stephens (1985), *Powder Technol.* **41**, 147-158

Savage & Lun (1988) *J. Fluid Mech.* **189**, 311-335

Dolgunin & Ukolov (1995) *Powder Technol.* **83**, 95-103

Gray & Thornton (2005) *Proc. Roy. Soc. A.* **461**, 1447-1473.

Gray & Chugunov (2006) *J. Fluid Mech.* **569**, 365-398.

Fan & Hill (2011) *New J. Phys.* **13**, 095009. (fluctuation induced)

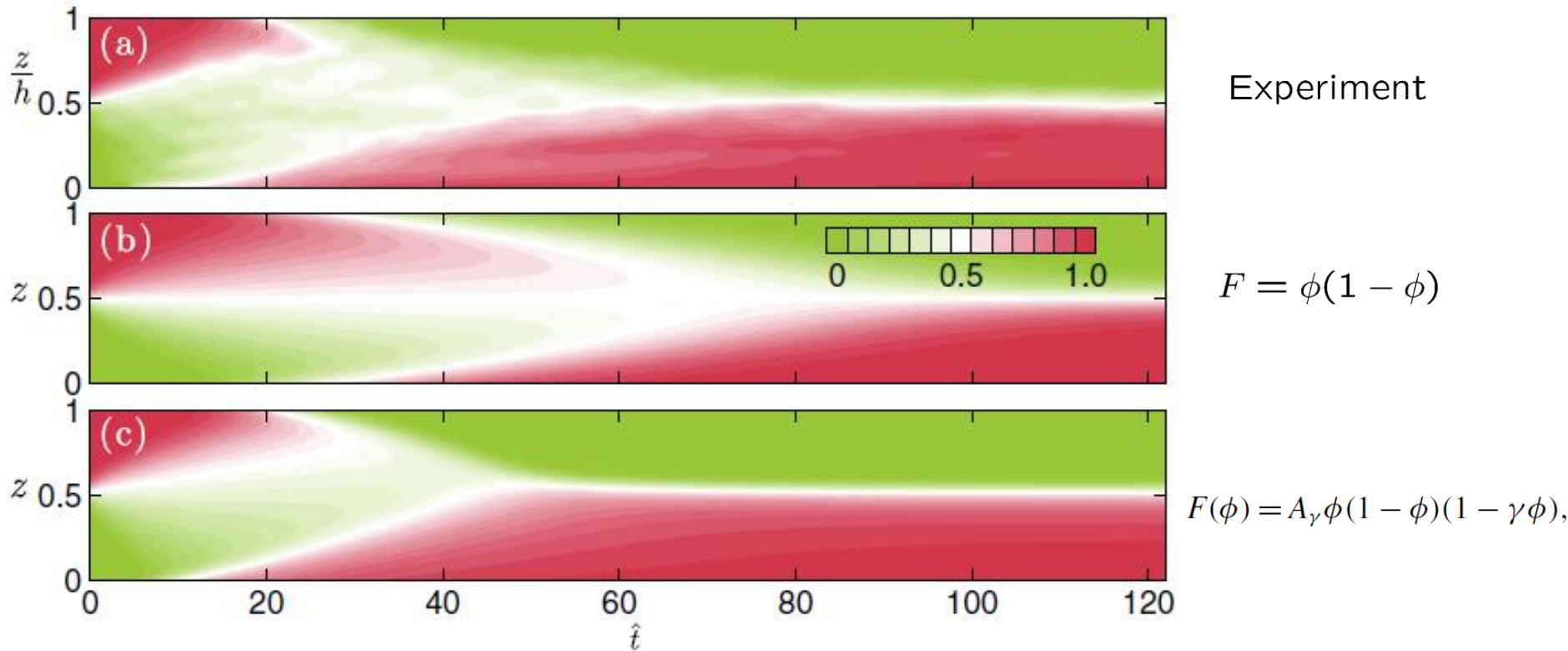
Gray & Ancy (2011) *J. Fluid Mech.* **678**, 535-558. (multiple sizes)

Gajjar & Gray (2014) *J. Fluid Mech.* **757**, 297-329. (asymmetry)

Gray & Ancy (2015) *J. Fluid Mech.* **779**, 622-668. (size and density)

$$\phi^s = \phi, \quad \phi^l = 1 - \phi$$

Cubic flux with  $\gamma=0.89$  captures slower rise of individual large particles, as well as their enhanced collective motion



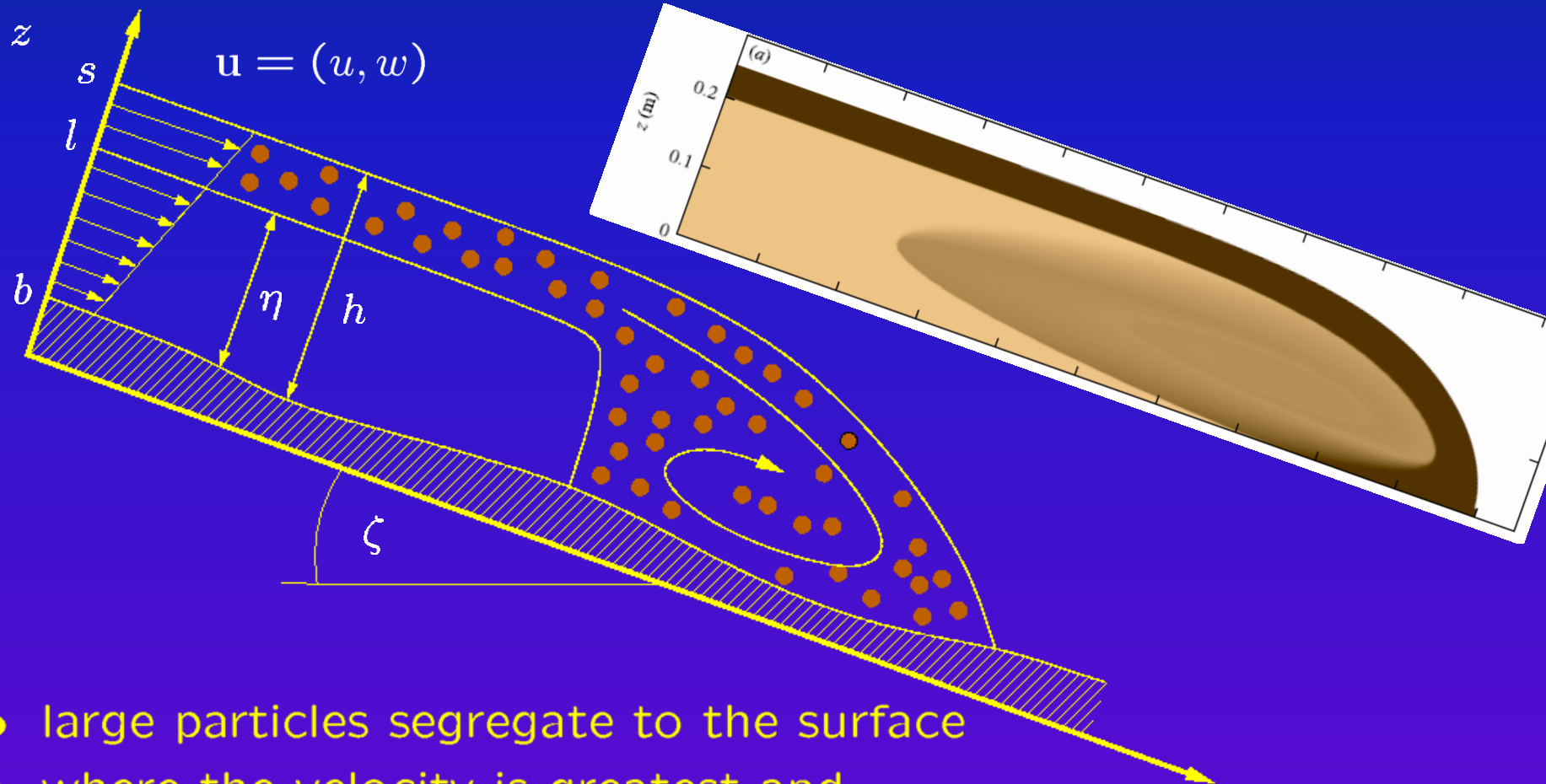
Gollick & Daniels (2009) *Phys. Rev E* **80**, 042301.

van der Vaart, Gajjar, Epely-Chauvin, Andreini, Gray & Ancey (2015) *Phys. Rev Lett.* **114**, 238001

Gajjar & Gray (2014) *J. Fluid Mech.* **757**, 297-329.

Gray (2018) *Annual Review Fluid Mech.* **50**, 407-433.

## Transport and accumulation of large particles



- large particles segregate to the surface
- where the velocity is greatest and
- are transported to the flow front where they are
- over run and recirculated by particle size segregation

## A depth averaged theory for particle size segregation

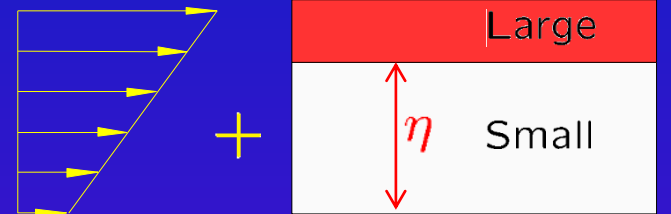
- Integrating the segregation-remixing equation w.r.t  $z$
- subject to the no flux and kinematic boundary conditions gives

$$\frac{\partial}{\partial t}(h\bar{\phi}) + \frac{\partial}{\partial x}(h\bar{\phi u}) = 0$$

- where the integrals evaluated assuming

$$h\bar{\phi} = \int_b^s \phi^s dz = \eta$$

$$h\bar{\phi u} = \int_b^s \phi^s u dz = \eta \bar{u} - (1 - \alpha) \bar{u} \eta \left(1 - \frac{\eta}{h}\right)$$



i.e. linear velocity with basal slip and sharp segregation

- This yields the large particle transport equation

$$\frac{\partial \eta}{\partial t} + \frac{\partial}{\partial x}(\eta \bar{u}) - \frac{\partial}{\partial x} \left( (1 - \alpha) \bar{u} \eta \left(1 - \frac{\eta}{h}\right) \right) = 0.$$

- for the evolution of the inversely graded shock interface  $\eta$ .

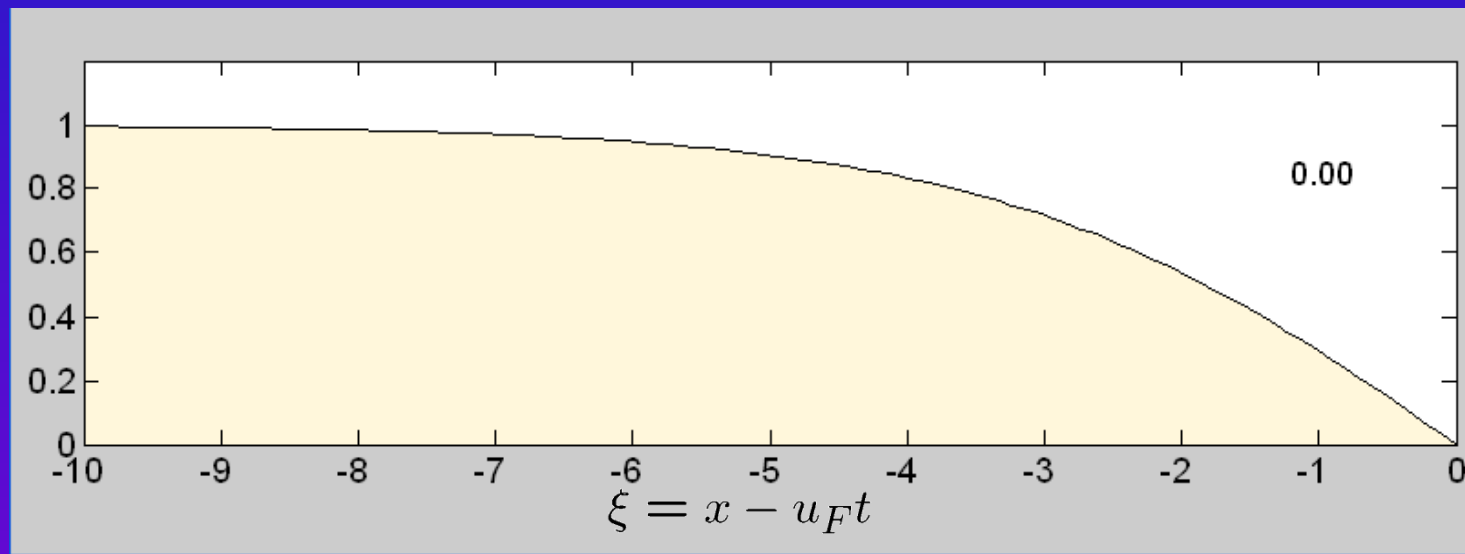
- Using  $\eta = h\bar{\phi}$  this can also be rewritten as

$$\frac{\partial}{\partial t}(h\bar{\phi}) + \frac{\partial}{\partial x}(h\bar{\phi}\bar{u}) - \frac{\partial}{\partial x}((1 - \alpha)h\bar{u}\bar{\phi}(1 - \bar{\phi})) = 0.$$

- Remarkably similar to the segregation equation ...

$$\frac{\partial \phi}{\partial t} + \frac{\partial}{\partial x}(\phi u) + \frac{\partial}{\partial z}(\phi w) - S_{ls} \frac{\partial}{\partial z}(\phi(1 - \phi)) = \frac{\partial}{\partial z} \left( D_r \frac{\partial \phi}{\partial z} \right)$$

- Large grains transported forwards to form bouldery flow front



- more RESISTIVE larger particles  $\Rightarrow$  feedback on bulk flow

## Inviscid avalanche model for segregation-mobility induced fingers

- For avalanche thickness  $h$ , small particle thickness  $\eta$  and depth-averaged velocity  $\bar{\mathbf{u}}$  the 2D coupled model is

$$\frac{\partial h}{\partial t} + \text{div}(h\bar{\mathbf{u}}) = 0,$$

$$\frac{\partial \eta}{\partial t} + \text{div} \left( \eta\bar{\mathbf{u}} - (1 - \alpha)\eta \left( 1 - \frac{\eta}{h} \right) \bar{\mathbf{u}} \right) = 0,$$

$$\frac{\partial}{\partial t}(h\bar{\mathbf{u}}) + \text{div}(h\bar{\mathbf{u}} \otimes \bar{\mathbf{u}}) + \text{grad} \left( \frac{1}{2}gh^2 \cos \zeta \right) = hg\mathbf{S},$$

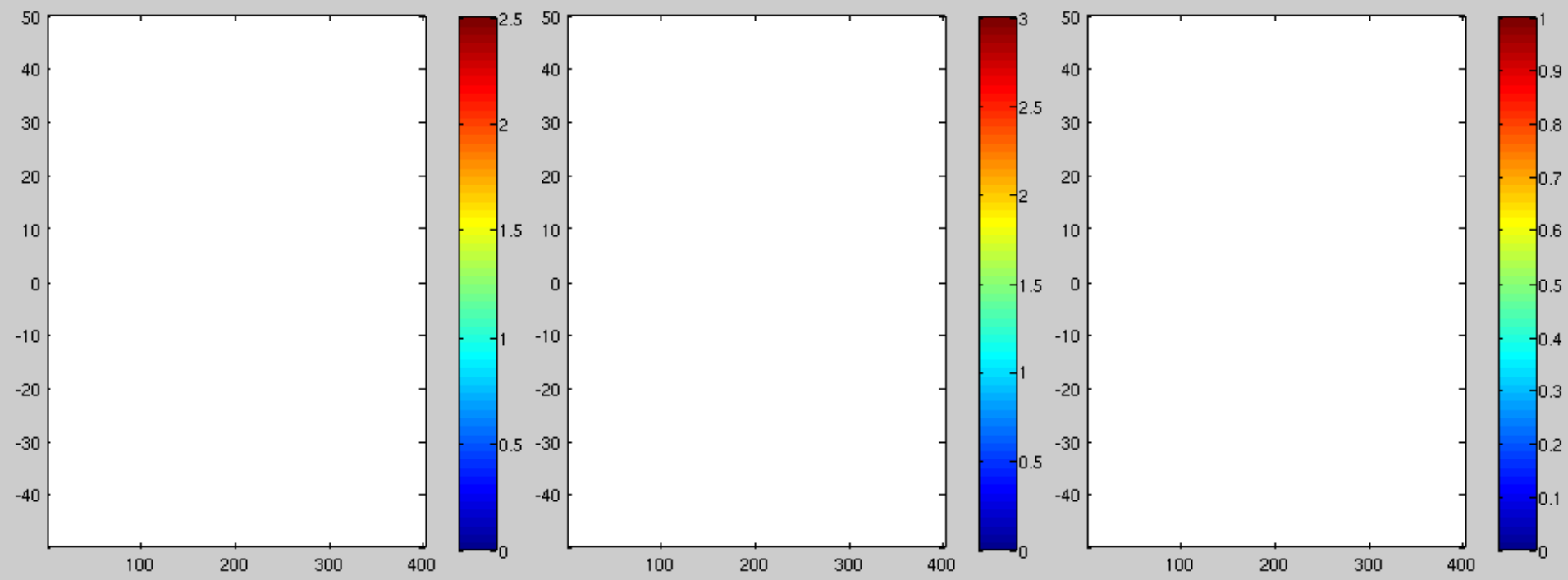
- source terms composed of gravity and basal friction

$$\mathbf{S} = \begin{pmatrix} \sin \zeta - \mu(\bar{u}/|\bar{\mathbf{u}}|) \cos \zeta, \\ -\mu(\bar{v}/|\bar{\mathbf{u}}|) \cos \zeta, \end{pmatrix}$$

- coupling through  $\bar{\phi} = \eta/h$  dependent friction coefficient

$$\mu = (1 - \bar{\phi}) \mu^L + \bar{\phi} \mu^S, \quad \mu^L > \mu^S$$

t=0.00



$h$

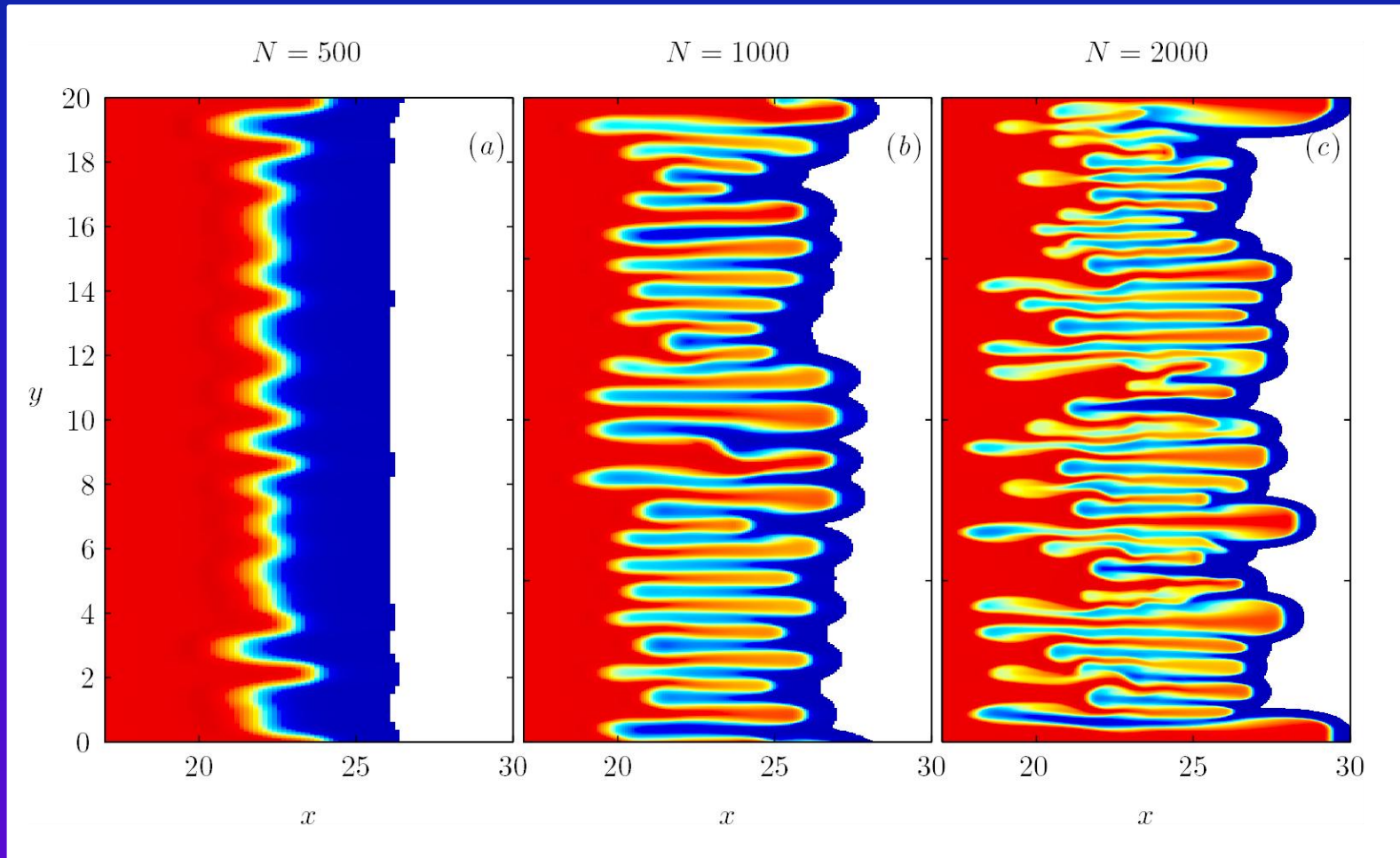
$|\bar{u}|$

$\bar{\phi}$

- The model is hyperbolic
- captures the instability mechanism
- and forms large rich lateral levees, BUT ....

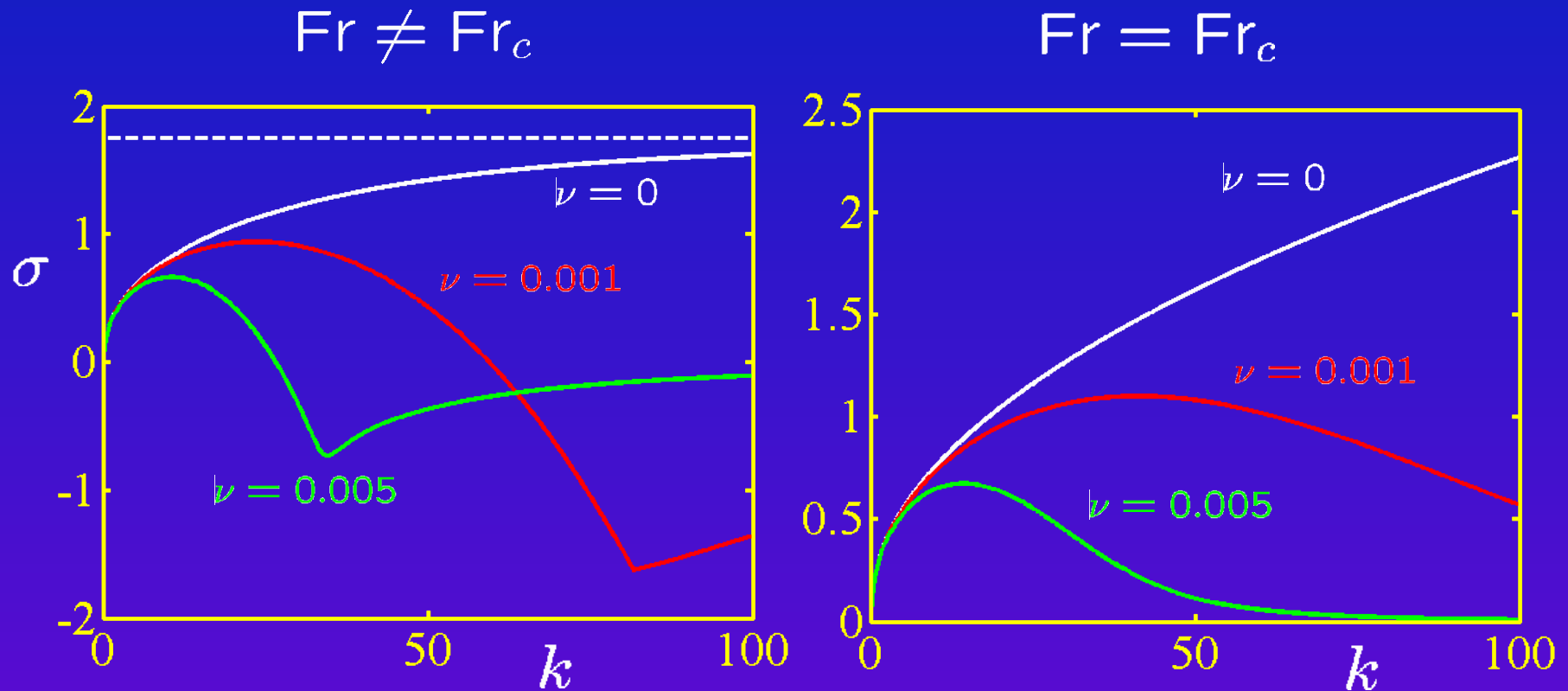


## Numerical solutions are grid dependent ...!



- Numerical viscosity is setting the wavelength  
⇒ there is some important missing physics

- cause of problem is that the equations are ill-posed for one value of the concentration, when  $Fr_c = [(1 - \alpha)|2\eta_0 - 1|]^{-1}$ , i.e. linear instability growth rate tends to infinity



- introducing a physically based viscosity can solve the problem, BUT what is that physics?

## A two-dimensional fully coupled model including rheology

- Adding a two-dimensional depth-averaged  $\mu(I)$ -rheology implies a system of conservation laws of the form

$$\frac{\partial h}{\partial t} + \text{div}(h\bar{\mathbf{u}}) = 0,$$

$$\frac{\partial \eta}{\partial t} + \text{div} \left( \eta\bar{\mathbf{u}} - (1 - \alpha)\eta \left( 1 - \frac{\eta}{h} \right) \bar{\mathbf{u}} \right) = 0,$$

$$\frac{\partial}{\partial t}(h\bar{\mathbf{u}}) + \text{div}(h\bar{\mathbf{u}} \otimes \bar{\mathbf{u}}) + \text{grad} \left( \frac{1}{2}h^2g \cos \zeta \right) = hg\mathbf{S} + \text{div} \left( \nu h^{\frac{3}{2}}\bar{\mathbf{D}} \right),$$

- where the two-dimensional strain-rate tensor is

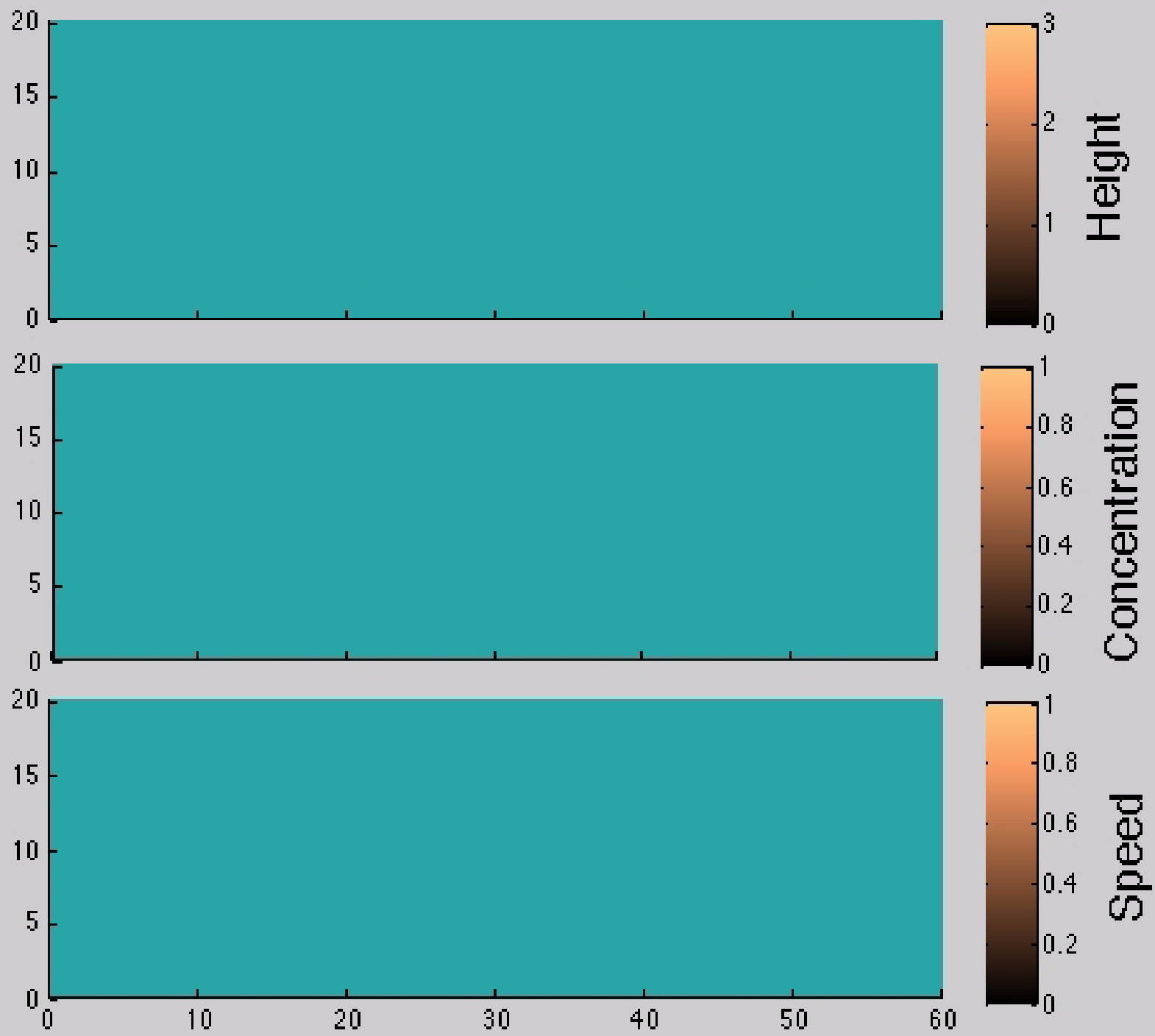
$$\bar{\mathbf{D}} = \frac{1}{2} (\nabla \bar{\mathbf{u}} + \nabla \bar{\mathbf{u}}^T)$$

- the coefficient  $\nu$  in the viscosity  $\nu h^{1/2}/2$  is determined from the friction law

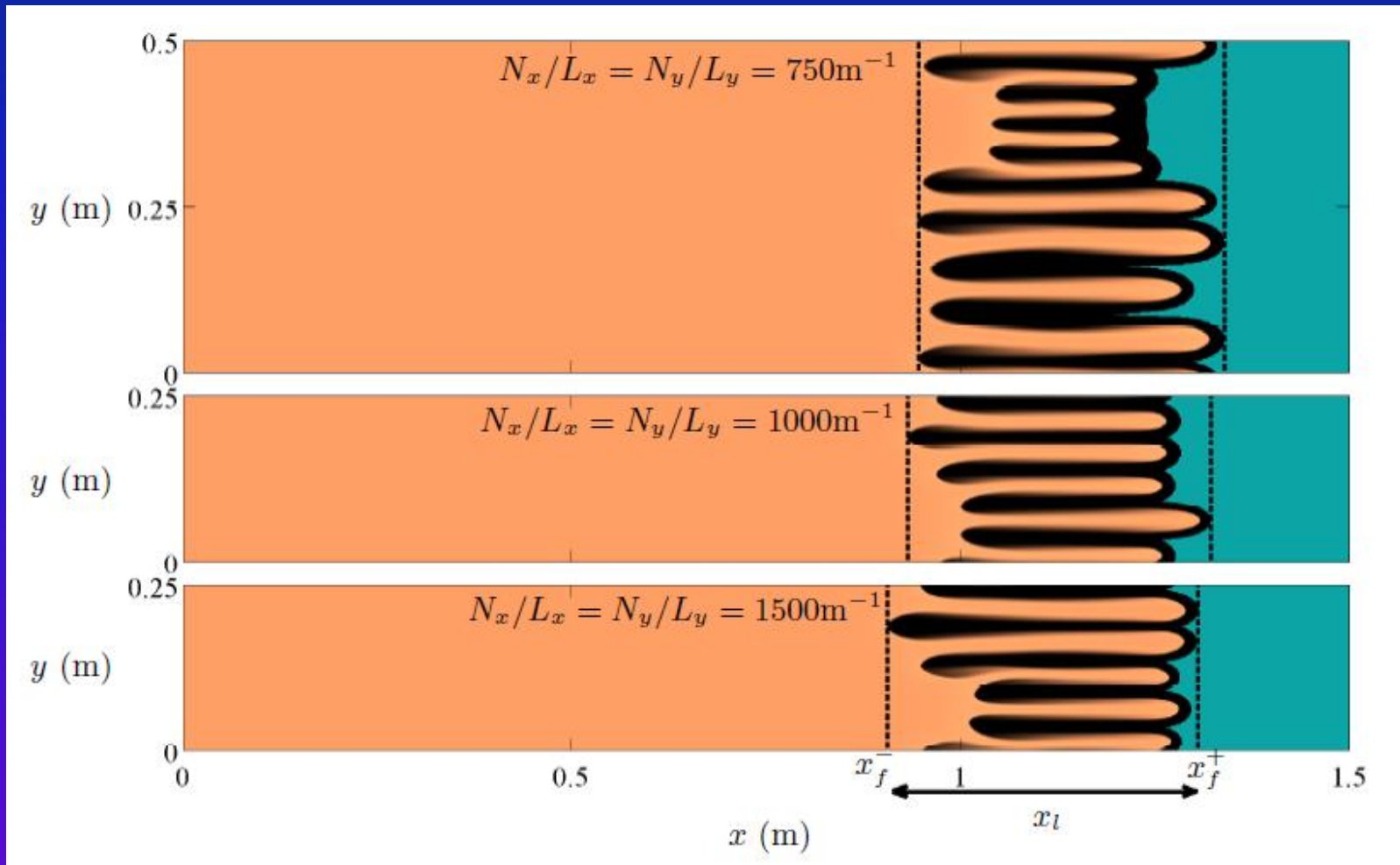
Baker, Barker & Gray (2016) *J. Fluid Mech.* **787**, 367-395.

Baker, Johnson & Gray *J. Fluid Mech.* **809**, 168-212.





## The depth-averaged $\mu(I)$ -rheology is crucial for grid resolved fingers



- We have grid convergence!
- However, still can't bring levees fully to rest
- We don't understand the viscosity of mixtures of grain sizes

## The $\mu(I)$ -rheology for liquid-like granular flows

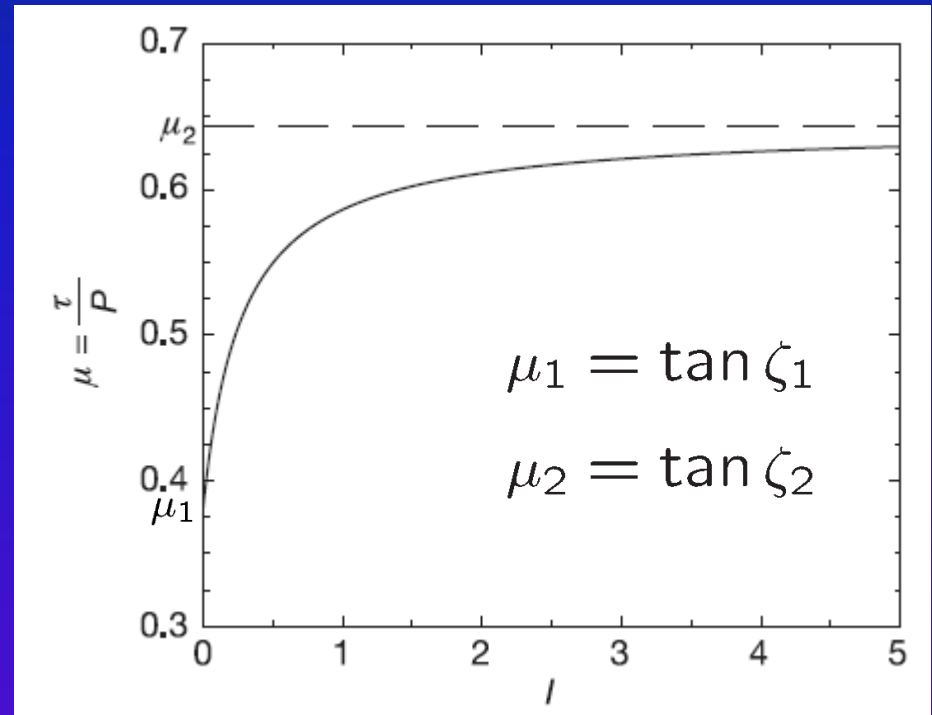
- GDR MIDI (2004) and Jop *et al.* (2006): proposed constitutive law

$$\boldsymbol{\tau} = \mu(I)p \frac{\mathbf{D}}{\|\mathbf{D}\|}$$

- where 2nd invariant

$$\|\mathbf{D}\| = \sqrt{\frac{1}{2} \text{tr} \mathbf{D}^2}$$

- If  $\mu = \text{const}$  this reduces to Drucker-Prager



- BUT, friction  $\mu$  is a function of the inertial number  $I$

$$\mu(I) = \mu_1 + \frac{\mu_2 - \mu_1}{I_0/I + 1}, \quad I = \frac{2\|\mathbf{D}\|d}{\sqrt{p/\rho^*}}$$

- where  $d$  is the particle diameter and  $\rho^*$  is the intrinsic density.

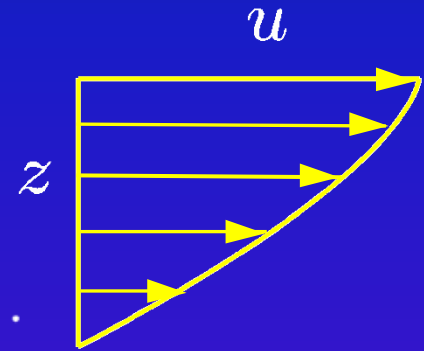
## The depth-averaged $\mu(I)$ -rheology for granular flows

Gray & Edwards (2014) *J. Fluid Mech.* **755**, 503-534.

- Steady-uniform flow has constant inertial number, a lithostatic pressure and Bagnold velocity

$$I = I_\zeta, \quad p = \rho g(h - z) \cos \zeta.$$

$$u = \frac{2I_\zeta}{3d} \sqrt{\Phi g \cos \zeta} \left( h^{3/2} - (h - z)^{3/2} \right).$$



- Depth-averaging the inviscid avalanche equations emerge naturally at first order with basal friction law

$$\mu_b(h, Fr) = \mu_1 + \frac{\mu_2 - \mu_1}{\beta h / (L Fr) + 1}, \quad Fr > \beta,$$

- This is just Pouliquen & Forterre's (2002) law, where

$$Fr = \frac{|\bar{\mathbf{u}}|}{\sqrt{gh \cos \zeta}}$$

- Add in small in-plane deviatoric stress correction  $\tau_{xx}$
- evaluate using the steady-uniform Bagnold solution

$$\tau_{xx} = \mu(I)p \frac{D_{xx}}{\|\mathbf{D}\|} = 2\rho g \sin \zeta \left( h^{1/2}(h-z)^{1/2} - (h-z) \right) \frac{\partial h}{\partial x}.$$

- formal depth-integration gives

$$h\bar{\tau}_{xx} = \frac{1}{3}\rho g \sin \zeta h^2 \frac{\partial h}{\partial x}.$$

- Use depth-averaged Bagnold velocity  $\bar{u} = \frac{2I_\zeta}{5d} \sqrt{\Phi g \cos \zeta} h^{3/2}$  to convert to viscous-like term

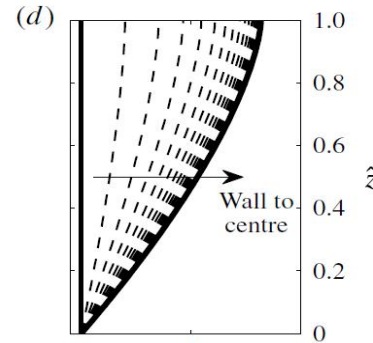
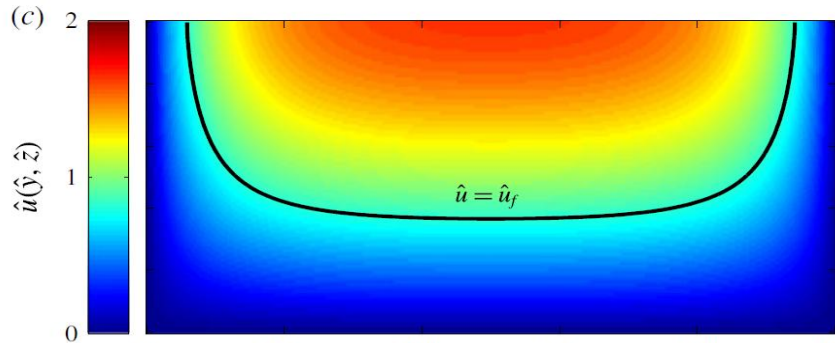
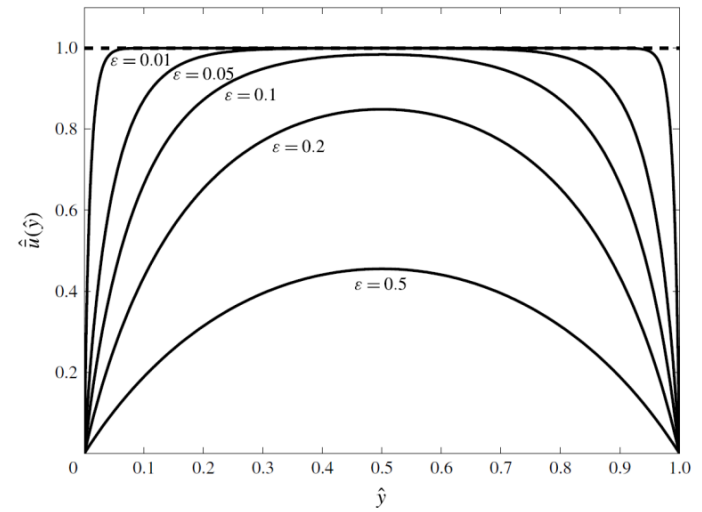
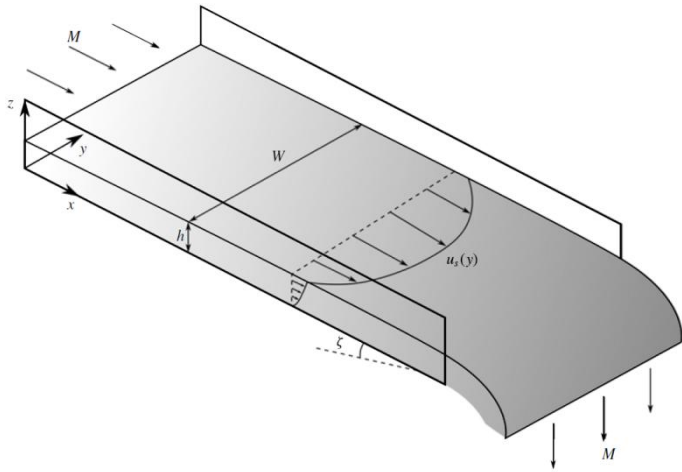
$$h\bar{\tau}_{xx} = \rho\nu h^{3/2} \frac{\partial \bar{u}}{\partial x}$$

- where angle dependent coefficient  $\nu$  is determined

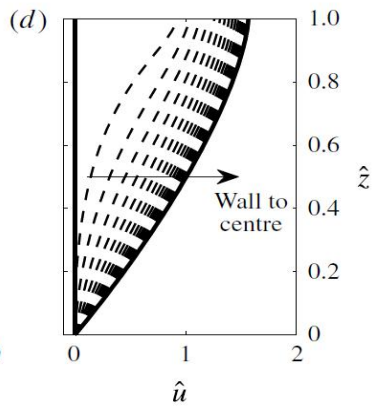
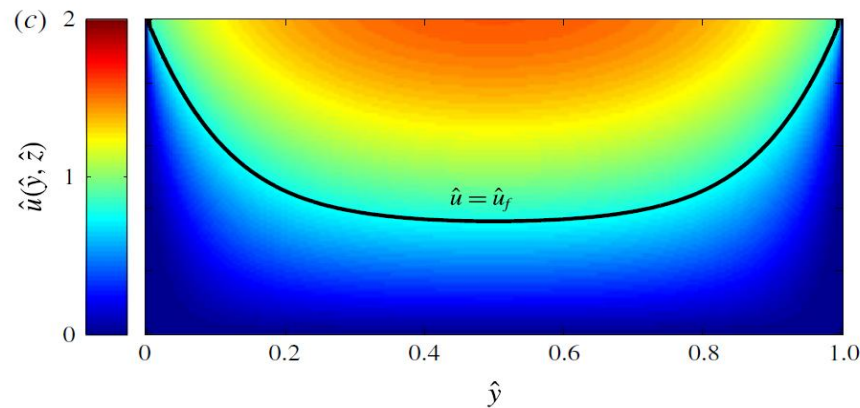
$$\nu = \frac{2L\sqrt{g}}{9\beta} \frac{\sin \zeta}{\sqrt{\cos \zeta}} \left( \frac{\mu_2 - \tan \zeta}{\tan \zeta - \mu_1} \right).$$



(a) cross-slope velocity profiles

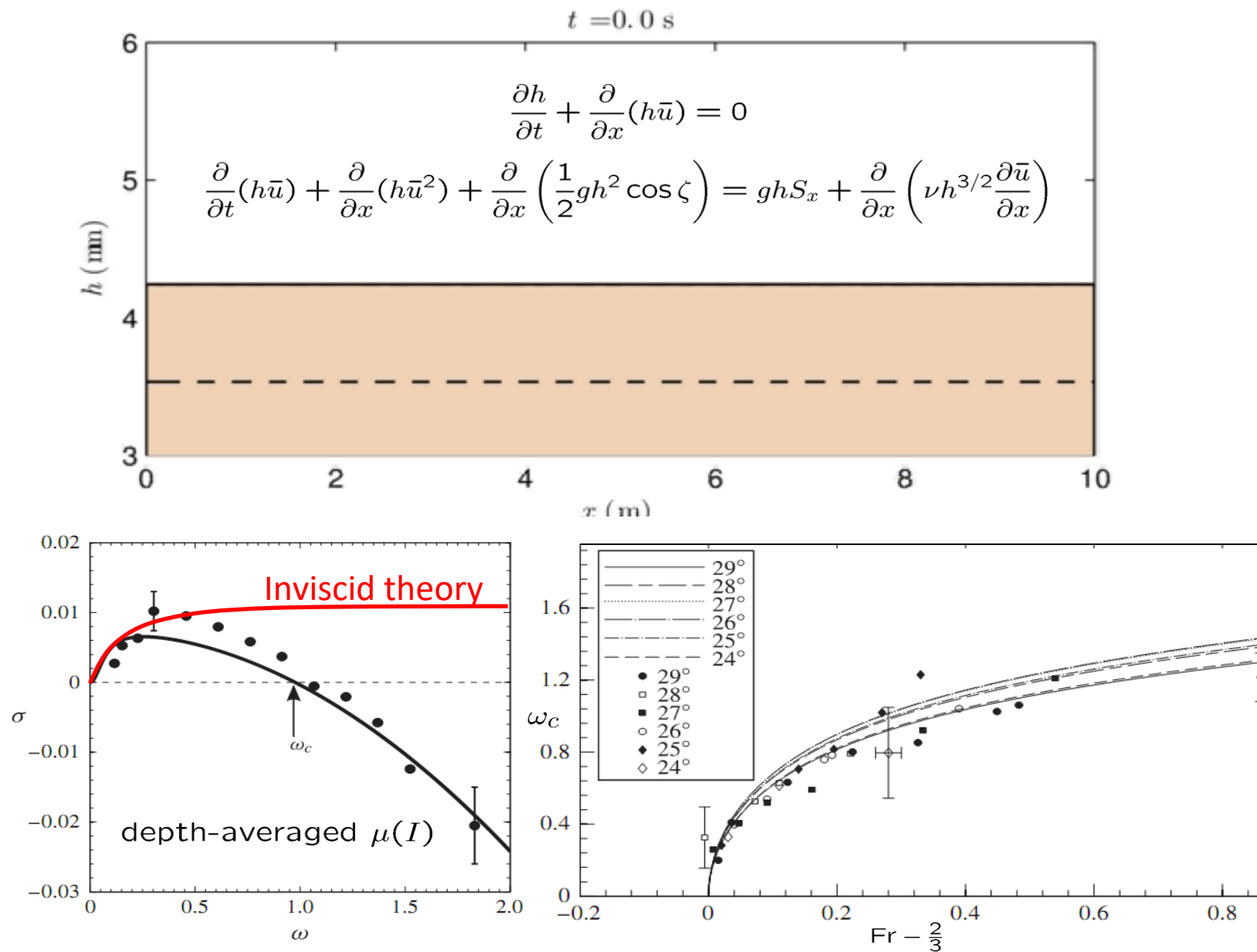


Reconstructed with Bagnold velocity profile



Steady 2D-solutions of full  $\mu(I)$ -rheology

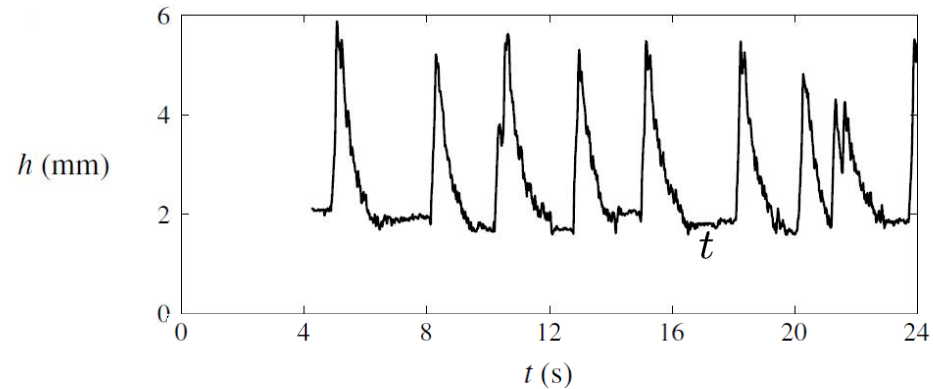
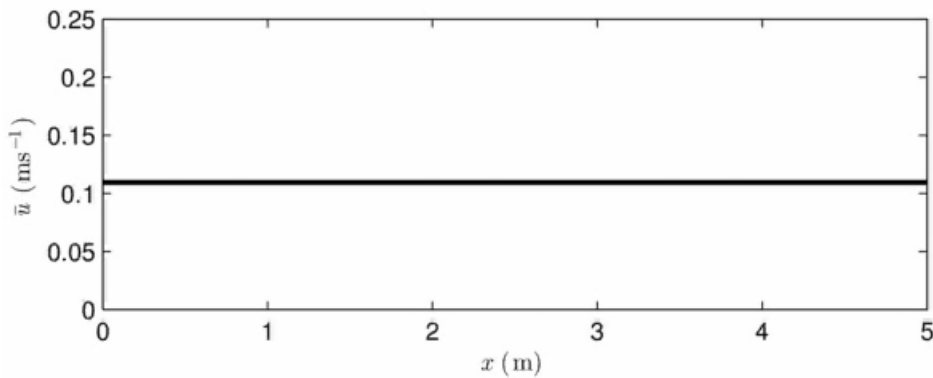
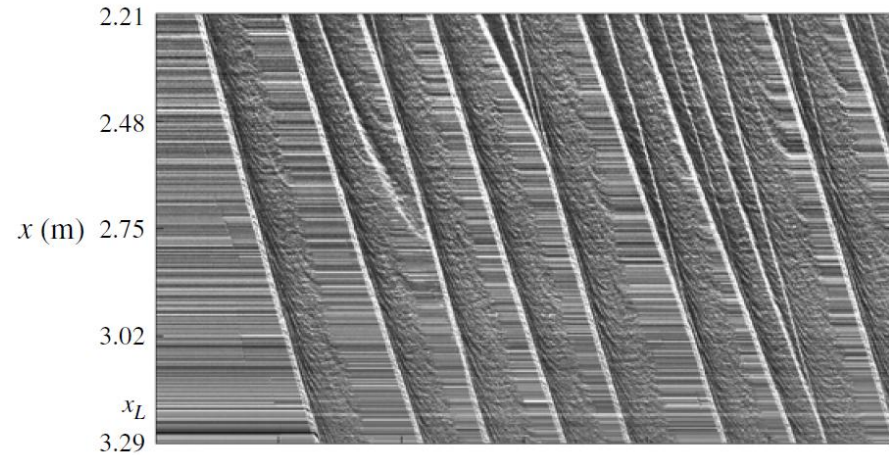
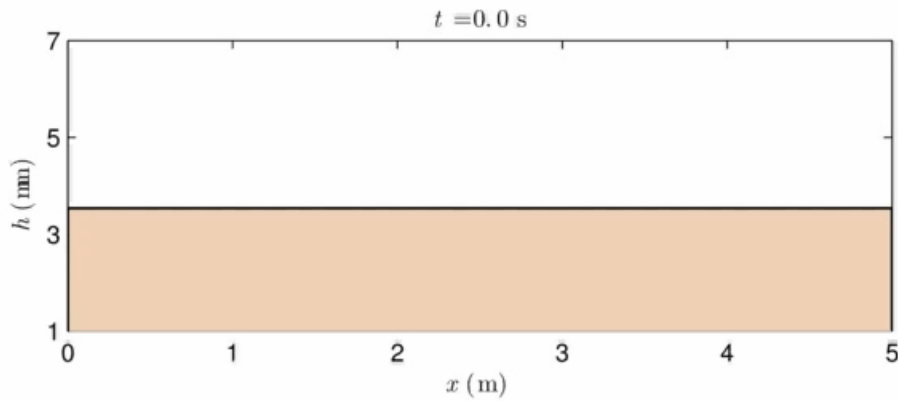
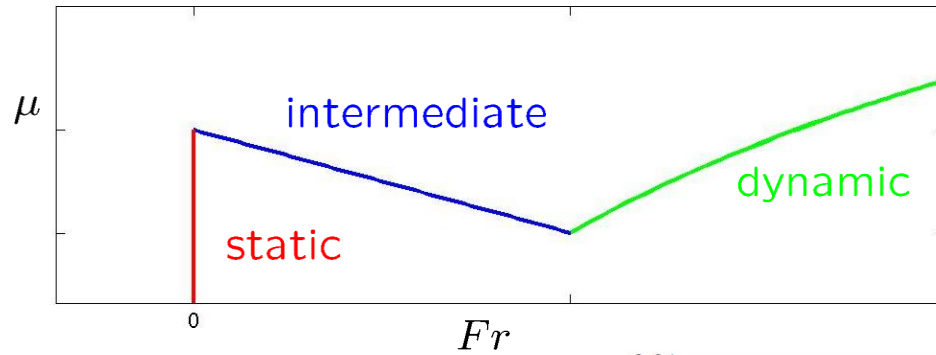
(b) Matches roll-wave cut-off frequency without any fitting parameters



Gray & Edwards (2014) *J. Fluid Mech.* **755**, 503-534.

Pouliquen & Forterre (2002) *J. Fluid Mech.* **453**, 133-151.

(c) Frictional hysteresis leads to erosion-deposition waves



Edwards & Gray (2015) *J. Fluid Mech.* **762**, 35-67.  
Pouliquen & Forterre (2002) *J. Fluid Mech.* **453**, 133-151.

similar waves  
spontaneously  
develop on  
erodible beds  
in the lab

there are  
static  
regions  
between  
wave crests

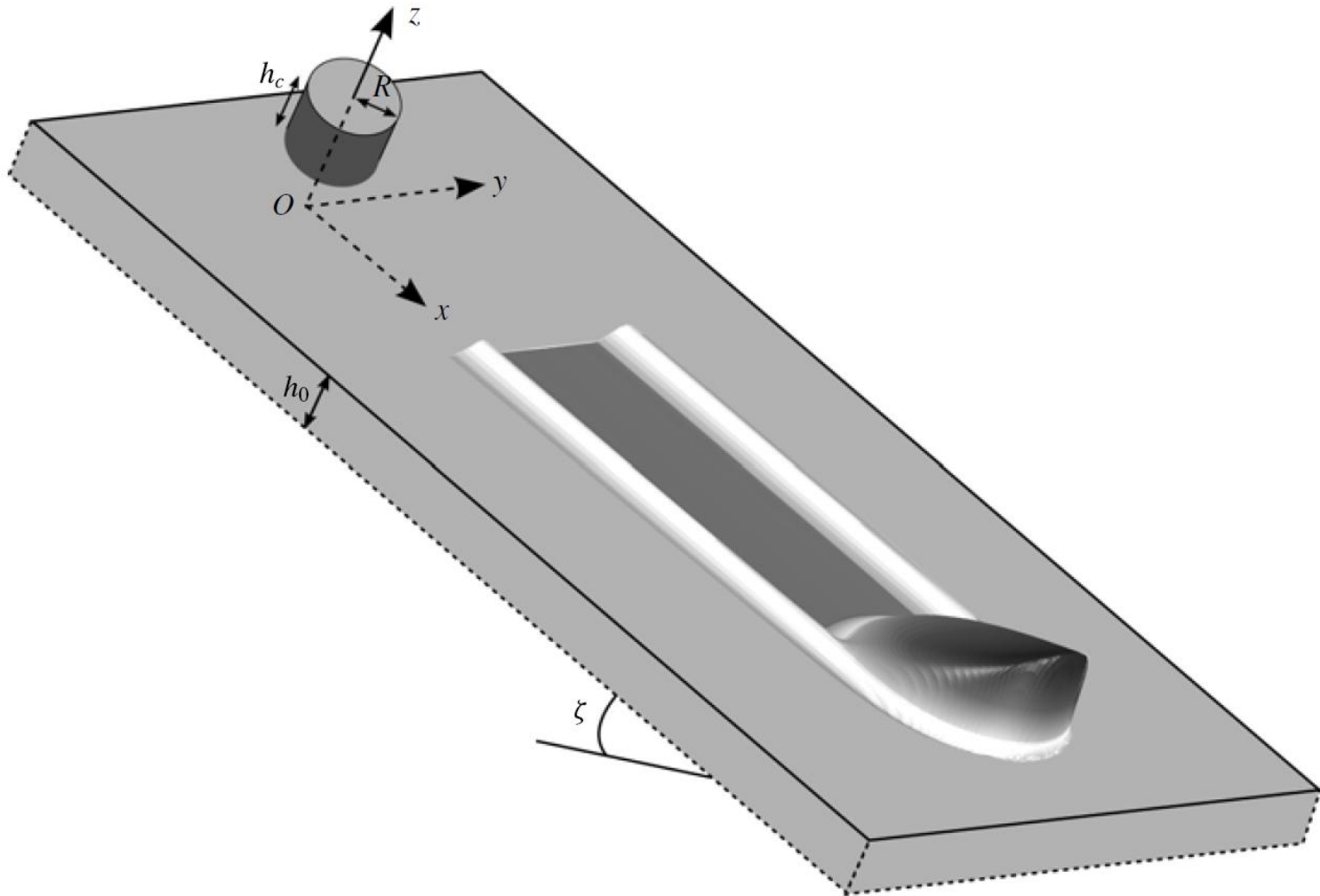
Daerr & Douady (1999)  
Borzsony *et al.* (2008)  
Takagi *et al.* (2011)



# Erosion-deposition waves in debris flows

SF-1

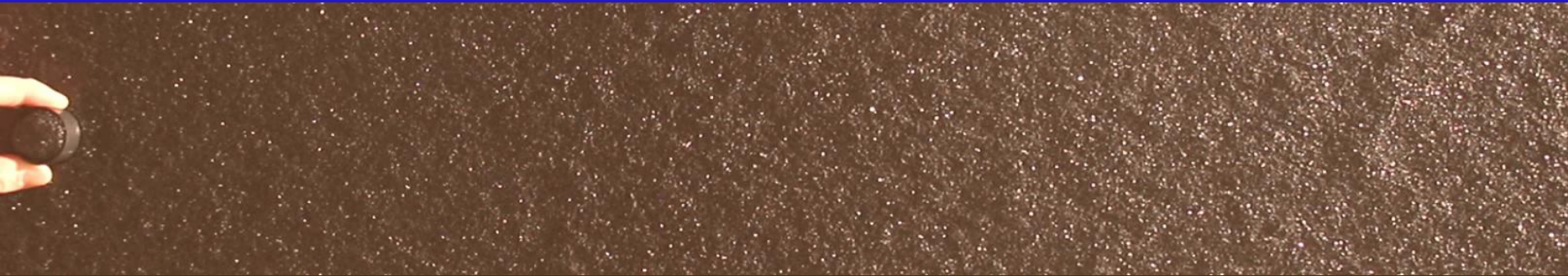
- 15<sup>th</sup> Oct 2000 an unintentional release of 150 000 m<sup>3</sup> water led to a debris flow in Fully Switzerland that had regular surges



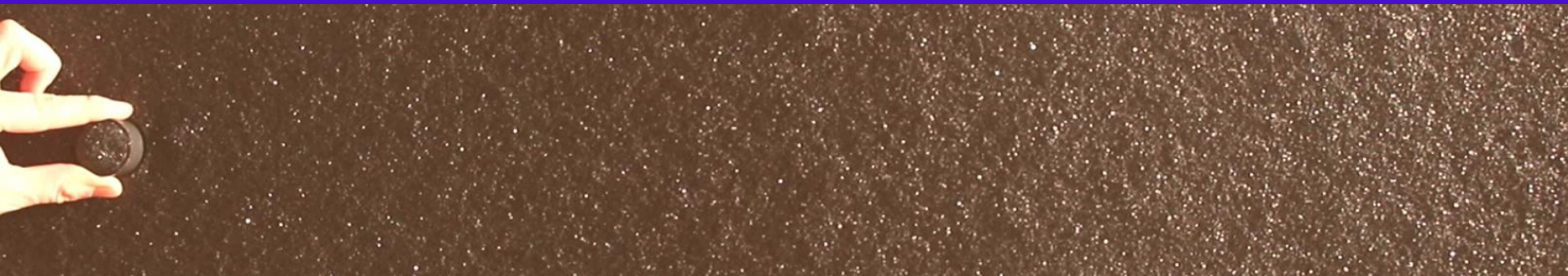
Edwards *et al.* (2017) Formation of levees, troughs and elevated channels by avalanches on erodible slopes, *J. Fluid Mech.* **823**, 278–315.



Growth



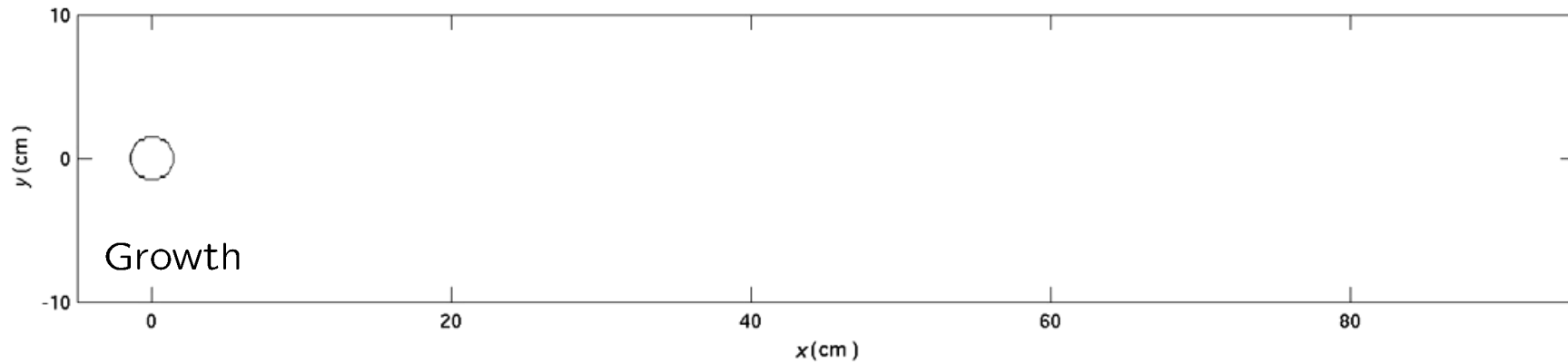
Steady Propagation



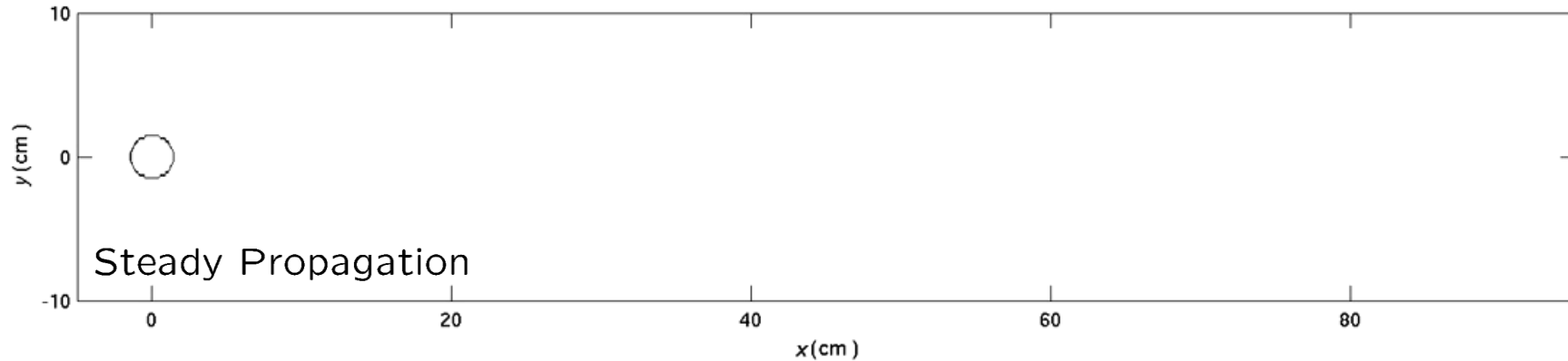
Decay

Edwards *et al.* (2017) Formation of levees, troughs and elevated channels by avalanches on erodible slopes, *J. Fluid Mech.* **823**, 278–315.

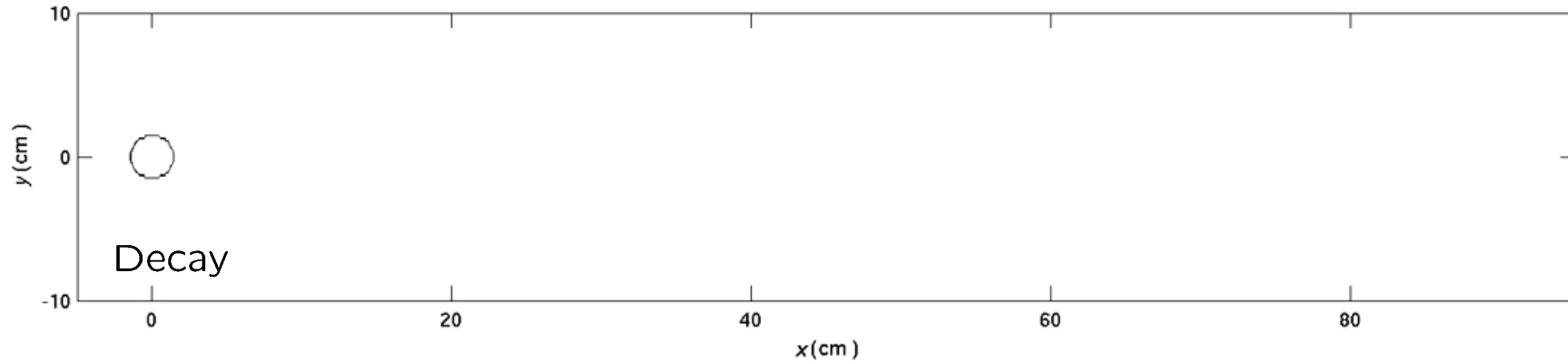
$t = 0.0 \text{ s}$



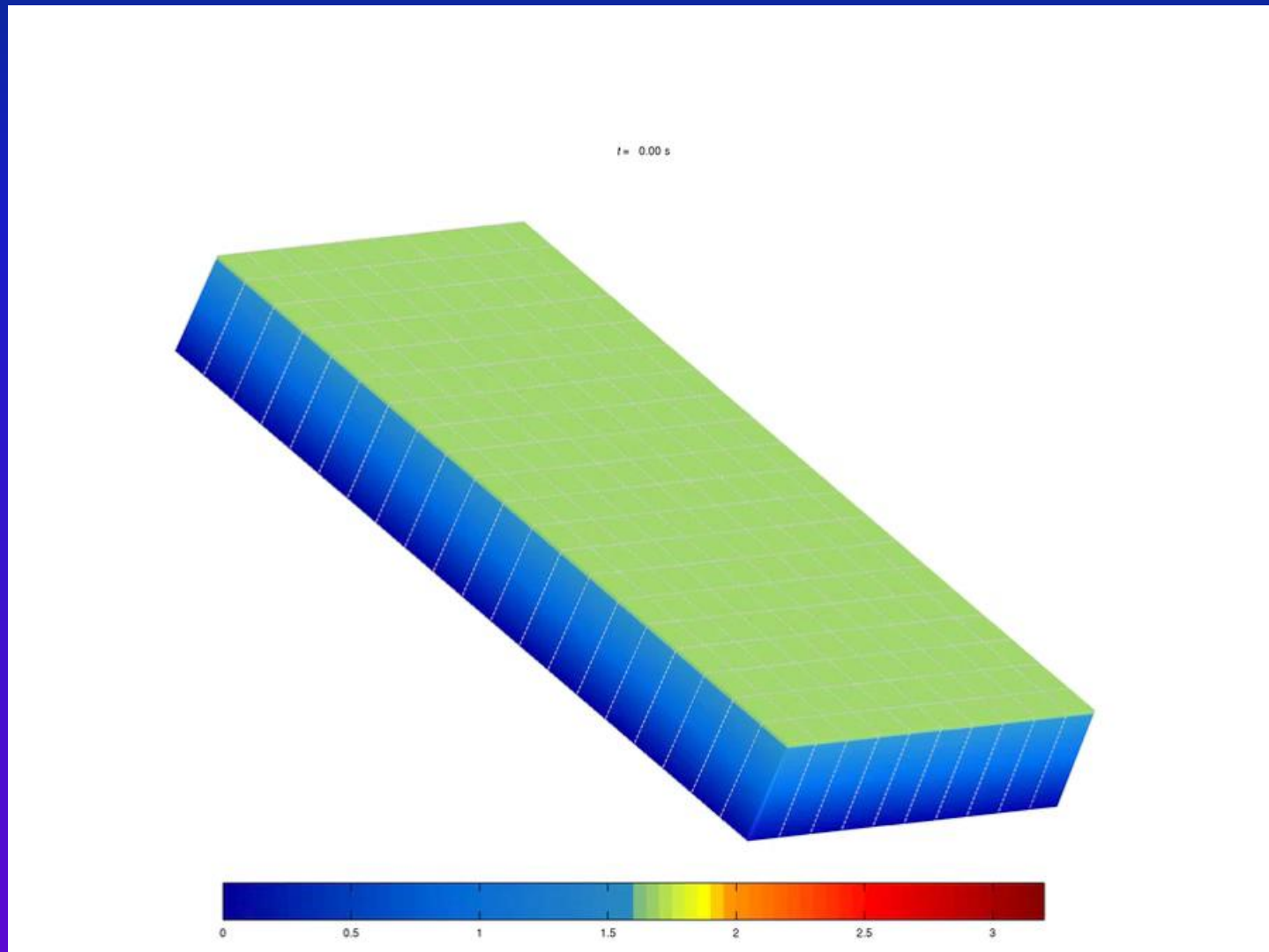
$t = 0.0 \text{ s}$



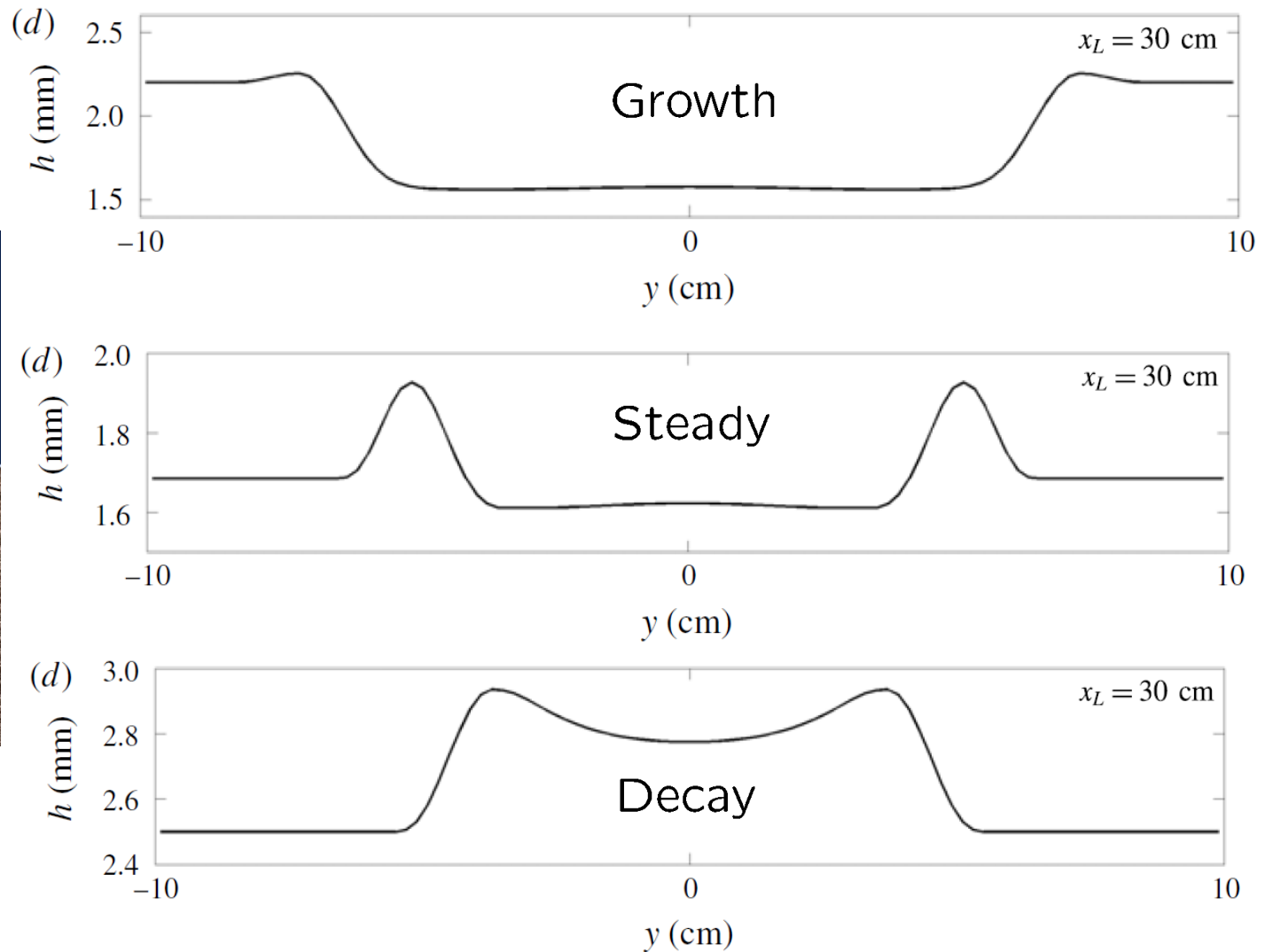
$t = 0.0 \text{ s}$







Edwards *et al.* (2017) Formation of levees, troughs and elevated channels by avalanches on erodible slopes, *J. Fluid Mech.* **823**, 278–315.



Edwards *et al.* (2017) Formation of levees, troughs and elevated channels by avalanches on erodible slopes, *J. Fluid Mech.* **823**, 278–315.